

ASHRAE STD 90.1 PARAGRAPH 6.5.6.1 READS:

"Exhaust air energy recovery. Individual fan systems that have both a design supply air capacity of 5,000 cfm or greater and have a minimum outdoor air supply of 70% or greater of the design supply air quantity shall have an energy recovery system with at least 50% energy recovery effectiveness." (The paragraph continues, supplying definitions and the requirement to bypass the heat recovery system during economizer operation)

Further in this section, an exception to these requirements is allowed for systems which require dehumidification. Specifically, subparagraph 6.5.6.1.i has exempted: "Systems requiring dehumidification that employ energy recovery in series with the cooling coil."

REASONS AND SUBSTANTIATION WHY THE HCU EXCEEDS ASHRAE STD 90

Section 6.5.6.1 ensures that whenever a system brings large amounts of outdoor air into a building, energy recovery equipment is in-place to minimize the energy required to heat or cool the incoming air.

At the same time, this section recognizes that different guidelines are needed when a system requires dehumidification. In those cases, exception (i) allows the use of energy recovery *not* from exhaust air, but rather from the waste heat of the incoming air stream itself. Figure 1 shows the series-configured heat recovery system allowed by exception (i).

The Munters HCU applies to that same situation: systems which require dehumidification, in which the energy for dehumidification can be recovered from within the system itself, without the parasitic effect of an overheated supply air stream.

The Munters HCU is exceptionally energy-efficient. On an annual basis, the system dries the air using 15 to 35% less energy than the exhaust air energy recovery system mandated by Section 6.5.6.1. It also uses 15 to 40% less energy than the dehumidification system allowed under exception (i).

Given that the intent of Std 90 is to reduce *annual* energy consumption, the HCU allows engineers to easily comply and exceed conditions of ASHRAE STD 90. Since the following demonstrates how the HCU exceeds STD 90, the HCU can be used to allow engineers to qualify for additional LEED points relating to increased building design efficiency.

DESICCANT DEHUMIDIFICATION USING CONDENSER HEAT FOR REACTIVATION

Desiccant dehumidifiers now serving more than 500 commercial and institutional buildings use site-recovered heat to reactivate (dry) the desiccant. They get this heat from the condenser section of an internal DX cooling system which pre-cools the air, as shown in figure 1. In this configuration, the desiccant system:

- 1. Removes moisture at a rate of 0.136 kw/lb/h including fans (Harriman & Judge, Dehumidification Equipment Advances, ASHRAE Journal March 2002, pp. 22-29).
- 2. Delivers air at, or slightly below the temperature set point of the conditioned space.

LESS ANNUAL ENERGY THAN COOLING COIL ASSISTED BY HEAT RECOVERY

From first appearances, it's not obvious why the Munters HCU could use less energy for dehumidification than the combination of an enthalpy heat exchanger and a cooling coil. But on examination, the reasons for this fact become clear.

The key difference is that the desiccant-assisted cooling coil is much more efficient for dehumidification than the baseline system, when moderate outdoor air temperatures combine with high moisture levels. These conditions occur for thousands of hours per year in all climate regions. As a consequence, on an annual basis, the desiccant-assisted coil uses less energy to do the same work as the same coil when assisted by an exhaust-air energy recovery system. The desiccant-assisted coil simply does not have to do as much work, because the desiccant component removes a great deal of the moisture.

The charts in figures 2, 3, 4 and 5 report the annual energy comparisons between the baseline system and our proposed exception.

The analysis assumes that both systems must deliver outdoor air to the building at a neutral moisture level (75°F, 50% rh, 28.01 Btu/lb, 55°F dpt, 65 gr/lb). A second assumption is that, because dehumidification is required, both systems must dry the incoming air any time the outdoor air is more humid than the building-neutral moisture level.

Note that at the extreme design condition, the exhaust recovery-assisted coil performs admirably, while the desiccant-assisted coil is at a disadvantage. However, those conditions, by definition, only occur for 35 to 175 hours every year. Shortly, as the outdoor temperature falls and the outdoor humidity rises, the desiccant-assisted coil becomes much more energy-efficient than the baseline system. This is because the deep-drying capability of the desiccant relieves its cooling coil of the need to chill the air deeply to provide dehumidification down to the building-neutral level.

Consider the changes in enthalpy shown in figure 1 for the baseline coil vs. the desiccant-assisted coil. Note that when air is entering from the weather at 75°F and 102 gr/lb, the coil in the baseline system must reduce the enthalpy by 8.37 Btu/lb.

Compare that work to the enthalpy reduction required of the coil in the desiccant alternative. Because the desiccant component can dry the air deeply, the cooling coil only needs to reduce the enthalpy of the incoming air by 6.80 Btu/lb. The desiccant component accomplishes the remaining dehumidification. Since the coil in the desiccant system can do less work, the cooling equipment in that system uses less energy during those hours.

The spreadsheets show the energy saved when these differences are calculated for all of the hours when the outdoor humidity is above the condition required inside the building. Please note from the last column in these spreadsheets, that the baseline system has an advantage (uses less energy) until the outdoor enthalpy declines to about 37 Btu/lb. As the outdoor enthalpy goes below that value, the desiccant-assisted coil picks up advantages. Because there are so many hours below that enthalpy in all locations, the net effect is that the desiccant-assisted coil uses considerably less energy each year than the baseline system from section 6.5.6.1.

HCU V. OTHER DESICCANT DEHUMIDIFICATION CONFIGURATIONS

Not all desiccant systems exceed the efficiency of the base energy recovery systems. Many are suited only to the deepdrying of specialty low-dew point applications where their higher-than usual energy requirements are justified by user benefits.

When using the HCU in lieu of energy recovery systems engineers need to consider the following:

- 1. "Systems requiring dehumidification..." The HCU is when used in system designs that require humidity control.
- 2. "...in which the reactivation energy is entirely site-recovered..." The HCU recaptures all of its reactivation energy from the condenser coil resulting in extremely efficient operation.
- 2. "...and which does not deliver the supply air above the space design temperature." Finally, the HCU is designed to deliver air well within the ASHRAE defined comfort zone as it relates to temperature and does not add a sensible cooling load to the space.

SUMMARY

The Munters HCU would allow building owners to comply with std 90, while continuously using the most energy-efficient means of removing large amounts of moisture from air. The HCU has been proven in use over the last four years on the rooftops of more than 500 buildings across the US.

Building owners and society as a whole would benefit by using the HCU to reduce the energy needed to accomplish dehumidification. Denying the use of the HCU would discourage the energy-efficient innovation that std 90 is intended to promote.

References

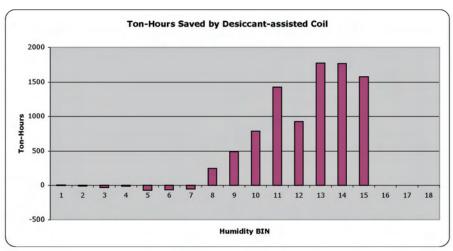
- 1) ASHRAE standard 90.1 Section 6.5.6.1 Exhaust air energy recovery
- 2) Harriman & Judge, Dehumidification Equipment Advances, ASHRAE Journal March 2002, pp. 22-29

Savings Estimate for Atlanta

Atlanta Weath	er (5 gr Hu	midity B	INs)
HR (gr/lb) MC	DB (°F) h (Btu/lb)	Hours
147.5	83.0	43.1	2
142.5	83.3	42.3	3
137.5	83.1	41.5	12
132.5	83.8	40.9	8
127.5	80.8	39.4	48
122.5	80.0	38.4	82
117.5	79.5	37.5	204
112.5	77.7	36.2	424
107.5	75.7	35.0	358
102.5	74.8	34.0	387
97.5	73.1	32.8	508
92.5	73.3	32.0	277
87.5	72.1	31.0	445
82.5	70.8	29.9	375
77.5	70.0	28.9	294
Total dehu	ımidificatio	n hours	3427

			Desiccant			
Exhaust Recover	y System (Baseli	ne)	Coil Work	Desiccar	nt Saving (or o	cost)
h (Entering Coil)	Coil Work (Ah)	Ton-Hours	(Ah)	Tons	Ton-Hours	%
35.56	12.95	34.0	15.95	(3.94)	(7.9)	-18.8%
35.16	12.55	49.4	15.15	(3.42)	(10.3)	-17.2%
34.76	12.15	191.3	14.35	(2.89)	(34.7)	-15.4%
34.46	11.85	124.4	13.75	(2.50)	(20.0)	-13.9%
33.71	11.10	699.0	12.25	(1.52)	(72.8)	-9.4%
33.21	10.60	1140.3	11.25	(0.86)	(70.5)	-5.8%
32.76	10.15	2716.3	10.35	(0.27)	(54.9)	-2.0%
32.11	9.50	5284.0	9.05	0.58	247.6	4.9%
31.51	8.90	4179.5	7.85	1.37	491.0	13.3%
31.01	8.40	4264.1	6.85	2.03	784.8	22.6%
30.41	7.80	5197.3	5.65	2.82	1430.2	38.0%
30.01	7.40	2688.5	4.85	3.34	925.3	52.5%
29.51	6.90	4027.1	3.85	4.00	1778.5	79.1%
28.96	6.35	3122.9	2.75	4.72	1769.4	130.7%
28.46	5.85	2255.4	1.75	5.37	1580.2	234.0%
Bas	seline ton-hours	35973.6	Annua	al Savings	8735.9	24.3%

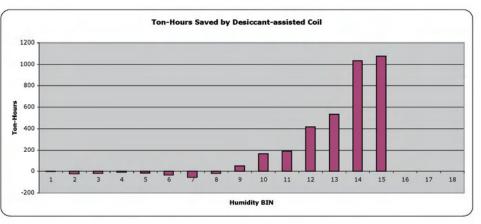
Assumptions Supply airflow Space DB 75 Space HR 55 Space enthalpy Exchanger Effectiveness Enthalpy leaving baseline coil Enthalpy leaving desiccant coil



	ather (5 gr H MCDB (°F) h		
152.5		43.6	1
147.5	85.3	43.6	6
142.5	84.8	42.7	6
137.5	80.3	40.8	4
132.5	82.4	40.5	8
127.5	82.0	39.7	21
122.5	83.1	39.2	42
117.5	81.5	38.0	37
112.5	77.3	36.2	86
107.5	76.6	35.2	132
102.5	75.2	34.1	98
97.5	75.2	33.3	168
92.5	75.1	32.5	177
87.5	72.6	31.1	263
82.5	71.7	30.1	235
77.5	70.2	28.9	396
72.5	69.0	27.9	310
Total de	humidificatio	n hours	1990

Savings Estimate	for Chicago					
	(5		Desiccant	Danisan	nt Caulma (au	
Exhaust Recovery Sys			Coil Work		nt Saving (or	
h (Entering Coil) Coil	Work (Ah)	Ton-Hours	(Ah)	Tons	Ton-Hours	%
35.81	13.20	17.3	16.45	(4.27)	(4.3)	-19.8%
35.81	13.20	103.9	16.45	(4.27)	(25.6)	-19.8%
35.36	12.75	100.4	15.55	(3.68)	(22.1)	-18.0%
34.41	11.80	61.9	13.65	(2.43)	(9.7)	-13.6%
34.26	11.65	122.3	13.35	(2.24)	(17.9)	-12.8%
33.86	11.25	309.9	12.55	(1.71)	(36.0)	-10.4%
33.61	11.00	606.1	12.05	(1.38)	(58.2)	-8.8%
33.01	10.40	504.8	10.85	(0.60)	(22.1)	-4.2%
32.11	9.50	1071.7	9.05	0.58	50.2	4.9%
31.61	9.00	1558.4	8.05	1.24	163.7	11.7%
31.06	8.45	1086.2	6.95	1.96	192.3	21.5%
30.66	8.05	1773.9	6.15	2.49	417.8	30.8%
30.26	7.65	1776.0	5.35	3.01	533.2	42.9%
29.56	6.95	2397.3	3.95	3.93	1033.8	75.8%
29.06	6.45	1987.9	2.95	4.59	1078.0	118.5%
28.46	5.85	3037.9	1.75	5.37	2128.4	234.0%
27.96	5.35	2174.7	0.75	6.03	1869.6	612.7%
Baseline	ton-hours	18690.9	Annua	al Savings	7271.2	38.9%

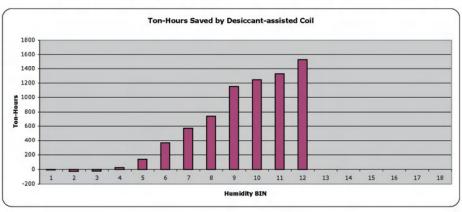
Assumptions	
Supply airflow	3500
Space DB	75
Space HR	65
Space enthalpy	28.01
Exchanger Effectiveness	0.5
Enthalpy leaving baseline coil	22.61
Enthalpy leaving desiccant coil	27.15



Newark Weath	er (5 ar Hu	midity RTNs	
HR (gr/lb) MC			
127.5	77.6	38.6	5
122.5	80.5	38.5	27
117.5	80.6	37.7	59
112.5	79.8	36.8	136
107.5	76.5	35.2	111
102.5	76.0	34.3	199
97.5	75.3	33.3	230
92.5	75.1	32.5	246
87.5	72.7	31.1	293
82.5	72.3	30.2	275
77.5	71.6	29.3	260
72.5	71.0	28.4	268
Total dehu	ımidificatio	n hours	2109

Exhaust Recovery	System (Baseline)		Desiccant Coil Work	Desiccar	nt Saving (or	cost)
h (Entering Coil)	Coil Work (Ah)	Ton-Hours	(Ah)	Tons	Ton-Hours	%
33.31	10.70	70.2	11.45	(0.99)	(5.0)	-6.6%
33.26	10.65	377.2	11.35	(0.93)	(25.0)	-6.2%
32.86	10.25	793.3	10.55	(0.40)	(23.6)	-2.9%
32.41	9.80	1748.4	9.65	0.19	25.9	1.5%
31.61	9.00	1310.5	8.05	1.24	137.7	11.7%
31.16	8.55	2231.8	7.15	1.83	364.4	19.5%
30.66	8.05	2428.6	6.15	2.49	572.1	30.8%
30.26	7.65	2468.4	5.35	3.01	741.0	42.9%
29.56	6.95	2670.8	3.95	3.93	1151.8	75.8%
29.11	6.50	2344.3	3.05	4.52	1243.4	113.0%
28.66	6.05	2062.9	2.15	5.11	1329.2	181.2%
28.21	5.60	1968.0	1.25	5.70	1528.4	347.6%
Bas	seline ton-hours	20474.4	Annu	al Savings	7040.1	34.4%

Assumptions	
Supply airflow	3500
Space DB	75
Space HR	65
Space enthalpy	28.01
Exchanger Effectiveness	0.5
Enthalpy leaving baseline coil	22.61
Enthalpy leaving desiccant coil	27.15



Tampa Weath			
147.5	85.0	43.6	2
142.5	84.1	42.6	13
137.5	84.6	41.9	85
132.5	84.5	41.1	261
127.5	82.9	39.9	407
122.5	81.2	38.7	561
117.5	79.8	37.6	730
112.5	78.2	36.4	810
107.5	76.7	35.2	490
102.5	76.9	34.5	386
97.5	75.3	33.3	514
92.5	73.9	32.2	324
87.5	72.1	31.0	515
82.5	70.2	29.7	505
77.5	68.9	28.6	396
72.5	69.1	27.9	343

			Desiccant			
Exhaust Recovery Sys	stem (Baseline	2)	Coil Work	Desicca	nt Saving (or	cost)
h (Entering Coil) Coil	Work (Ah)	Ton-Hours	(A h)	Tons	Ton-Hours	%
35.81	13.20	34.6	16.45	(4.27)	(8.5)	-19.8%
35.31	12.70	216.6	15.45	(3.62)	(47.0)	-17.8%
34.96	12.35	1377.2	14.75	(3.16)	(268.3)	-16.3%
34.56	11.95	4091.9	13.95	(2.63)	(686.8)	-14.4%
33.96	11.35	6060.4	12.75	(1.84)	(750.5)	-11.0%
33.36	10.75	7911.7	11.55	(1.06)	(592.7)	-7.0%
32.81	10.20	9768.1	10.45	(0.33)	(244.3)	-2.4%
32.21	9.60	10200.7	9.25	0.45	366.8	3.7%
31.61	9.00	5784.9	8.05	1.24	607.8	11.7%
31.26	8.65	4379.8	7.35	1.70	656.1	17.6%
30.66	8.05	5427.4	6.15	2.49	1278.4	30.8%
30.11	7.50	3187.2	5.05	3.21	1039.7	48.4%
29.51	6.90	4660.6	3.85	4.00	2058.2	79.1%
28.86	6.25	4139.3	2.55	4.85	2449.1	144.9%
28.31	5.70	2960.0	1.45	5.57	2206.3	292.8%
27.96	5.35	2406.3	0.75	6.03	2068.6	612.7%

Savings Estimate for Tampa

Assumptions	
Supply airflow	3500
Space DB	75
Space HR	65
Space enthalpy	28.01
Exchanger Effectiveness	0.5
Enthalpy leaving baseline coil	22.61
Enthalpy leaving desiccant coil	27.15

Total dehumidification hours

